

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. (Original) A process for direct conversion, by catalytic cracking, of a light olefinic hydrocarbon feed comprising at least 80% by weight of hydrocarbons containing at most 12 carbon atoms for the production of propylene, said process comprising direct cracking of the feed on a supported catalyst comprising at least one zeolite comprising silicon and aluminum and having form selectivity, from the group constituted by zeolites with one of the following structure types: MEL, MFI; NES, EUO, FER, CHA, MFS, MWW, and from the following zeolites: NU-85, NU-86, NU-88 and IM-5, comprising circulating the feed at a temperature in the range about 480°C to 620°C in at least one reactor on a granular moving bed of said catalyst, extracting from the lower portion of the reactor, continuously or discontinuously, a flow of catalyst comprising a carbonaceous deposit, transferring said catalyst to a regeneration zone where it undergoes at least one controlled oxidation step, then downstream of the regeneration zone, re-introducing the catalyst comprising a reduced amount of carbonaceous deposit directly or indirectly into the upper portion of said reactor, the catalyst used being such that the zeolites from said group have a Si/Al ratio in the range 40 to 130.
2. (Original) A process according to claim 1, in which at least 80% by weight of the feed is derived directly from one or more hydrocarbon cracking units.
3. (Currently Amended) A process according to claim 1 ~~or claim 2~~, in which at least 10% by weight of the feed is derived directly from one or more Fischer-Tropsch synthesis units.
4. (Currently Amended) A process according to ~~one of claims 1 to 3~~ claim 1, in which the zeolite or zeolites of said group belong to the sub-group constituted by zeolites of structure type MEL, MFI and CHA.
5. (Currently Amended) A process according to ~~one of claims 1 to 4~~ claim 1, in which

the zeolite or zeolites of said group are of structure type MFI.

6. (Currently Amended) A process according to ~~one of claims 1 to 5~~ claim 1, in which the zeolite or zeolites of said group are constituted by ZSM-5 zeolite.

7. (Currently Amended) A process according to ~~one of claims 1 to 6~~ claim 1, in which the overall space velocity HSV is in the range 13 to 80h<sup>-1</sup>.

8. (Currently Amended) A process according to one of claims 1 to 7, in which the overall space velocity is in the range 33 to 60h<sup>-1</sup>.

9. (Currently Amended) A process according to ~~one of claims 1 to 8~~ claim 1, in which the residence time for the catalyst in the reaction zone is in the range 1 to 40 hours.

10. (Currently Amended) A process according to ~~one of claims 1 to 9~~ claim 1, in which the residence time for the catalyst in the reaction zone is in the range 2 to 18 hours.